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High temperature behavior of electrostatic precipitator ash from municipal solid waste combustors

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Abstract

Municipal solid waste (MSW) flue gas residues require further treatment prior to disposal or reuse, and vitrification is one of the main solidification-stabilization processes. This paper investigates the high temperature behavior of MSW flue gas residues, performed in laboratory experiments up to 1400°C, and coupled with thermogravimetric analyses, X-ray diffraction, chemical and electron microprobe analyses. Melting temperatures of electrostatic precipitator (ESP) ash are in the range of 1202-1272 °C, whereas semi-dry scrubber residues melt between 1900 and 2300 °C. We show that the mean liquidus temperature of flue gas residues can be simply evaluated from their CaO content, by using the CaO-SiO₂-Al₂O₃ ternary diagram. For ESP ash, the liquidus phase is a Zn-rich aluminous spinel, followed by anorthite at 1225 °C, and melilite at 1190 °C. The total mass loss reaches 18 wt.% at 1300 °C. Moreover, 90% of evaporation takes place below 1000 °C, linked to evaporation of C, Cl, S, Na, K, and of the toxic metals Hg, Cd, Pb, Cu. Due to the high partial pressure of chlorine during heating, chloride is the most probable form of evaporation for Cd, Pb, and Cu. However, most of Zn, Cr, Ni, Sb and Sn remain in the vitrified product.

Keywords: Fly ash; Vitrification; Melting temperature; Evaporation; Toxic metals

1. Introduction

Incineration is an efficient method for managing municipal solid wastes (MSW), achieving up to a 90 % volume reduction, a 60 to 75 % mass reduction, a destruction of pathogenic agents and a possible recovery of energy. Whatever MSW combustor used, combustion of MSW produces two kinds of solid residues: (i) bottom ashes recovered from the primary combustor, and (ii) residues recovered from the treatment of flue gas. Due to their high contents of pollutant elements [1-6], many studies have been devoted to the characterization of flue gas residues, and particularly of electrostatic precipitator (ESP) ashes. Since solid flue gas residues are subject to leaching during their storage [5,7-13], they are potentially toxic for the environment and thus require further treatment before their long-term disposal. The aim of this waste management is that the ash-like toxic material could be transformed into a durable solid with a minimal release of pollutants into the environment. The solidification-stabilization processes include (1) extraction using acid or other solvents, (2) cement-based processes and (3) vitrification (melting and solidification). The vitrification technology mainly consists in melting these hazardous ashes at approximately 1400 °C in a high-temperature furnace and cooling in order to solidify them again. Even if energetic costs are important, vitrification, by comparison with hydraulic binders, (1) reduces the volume of residue, (2) leads to complete destruction of toxic organic compounds, and (3) produces a relatively inert residue, constituted by glass and/or crystals, and known as slag. During the melting operation, the non-volatile metals are immobilized into the structure of the slag, whereas the volatile metals are mainly transferred by evaporation to the exhaust gas, and converted into gas cooler ash. According to the French legislation, the melted slags resulting from flue gas residues, previously considered as hazardous wastes, are now stored in disposals dedicated for inert wastes. Studies devoted to the long-term behavior of these slags are still in progress, and the use of melted slags as secondary raw materials like bottom ashes will depend on the obtained results. The kinetics of evaporation of Cd, Pb, Cu, Zn from a MSW fly ash were

determined in different atmospheres between 670 and 1300 °C [14,15]. Moreover, Sakai and Hiraoka [16] have investigated the distribution of metals between melted slag, gas cooler ash and bag filter ash obtained after direct melting of fly ashes at 1400 °C. Finally, leaching characteristics of melted slag have been documented by Lin and Chang [17]. However, only few data are available concerning element behavior of MSW flue gas residues coupled with their mineralogy during thermal treatment. In this study, thanks to high-temperature experiments performed with MSW flue gas residues, we evaluate the range of their melting temperatures and their high-temperature phase relationships, together with the elemental behaviour between 150 and 1400 °C, especially for pollutant metals.

2. Materials and methods

2.1. Experimental design

This study principally focused on electrostatic precipitator (ESP) ash resulting from direct electrofiltration of flue gas. These solid residues were sampled in a MSW combustion facility located in an urban area of 600 000 inhabitants in the southeast France, equipped with two parallel trains of 12 ton/h each. MSW is fed into the combustion chamber with a grate consisting of six rollers for each train. The ESP ashes were compared to another type of flue gas residues, a semi-dry scrubber residue (SDSR), obtained by semi-dry process, in which flue gas, after cooling, is cleaned by injection of a lime slurry into the scrubber. These SDSR residues come from a MSW combustion facility located in northeast France, equipped with two parallel trains, each having a nominal capacity rating of 6 ton/h, and a primary combustor with movable grates. The feed stream is composed of household waste collected from an area with 167 000 inhabitants. ESP ashes and SDSR correspond to aluminosilicate materials, rich in calcium and chlorine, and containing numerous pollutants (As, Cd, Cr, Hg, Ni, Pb, Zn...) from tens of µg/g to tens of thousands of µg/g. These

residues consist of a very heterogeneous assemblage of glasses, metals, and crystals in which pollutant elements are distributed [5].

In order to determine the factors that control the behavior of pollutant elements in MSW combustors, and during the vitrification process, several types of experiments were performed using ESP ashes. We first defined their mean liquidus temperature and their liquidus phases (Table 1). In addition, during the heating of these residues, total mass loss was monitored by thermogravimetric experiments, changes in the mineralogy by X-ray diffraction and elemental behavior by chemical analyses. Finally, a set of experiments was carried out above the liquidus temperature, in order to document the evaporation rate of the main pollutants during vitrification of these ESP ashes.

2.2. Raw material and sample preparation

The chemistry and the mineralogy of several ESP ashes, sampled during two distinct periods in one combustion facility located in southeast France have been documented in a previous paper [5]. Since one of the main results of this study was to demonstrate the low seasonal chemical and mineralogical variations, one representative ESP ash of this sampling, noted ESP 261, have been chosen (Table 2). Two to three kilos of this sample were collected directly at the base of the electrostatic filter, prior to the storage silo. Then 50 grams were taken and quartered, in order to ensure sample homogeneity, and finally ground to a grain size less than 70 μm . The same protocole was used to sample one representative SDSR in a facility located in northeast France, where flue gas are treated by a semi-dry process.

2.3. Experimental methods

All experiments were performed at atmospheric pressure in a Gero vertical drop-quench furnace, which can reach 1700 °C. Temperature was controlled using a Eurotherm

818 controller and measured by two independent Pt-PtRh₁₀ thermocouples located in the hotspot of the furnace.

For the determination of the melting temperature, aliquots of 50-100 mg of powdery starting material were pressed onto wire platinum loops, with a diameter of 0.10 mm, using polyvinyl alcohol as a binder. The sample was introduced into the center of the tube furnace, and directly heated at the dwell temperature. After each experiment and in order to frozen in the high temperature phase relations, the sample was drop-quenched in water at a quenching rates of the order of 500°C.s⁻¹. It was then mounted as polished sections for optical determination and/or electron-microprobe analyses.

The thermogravimetric analysis (TGA) measurements were carried out on a Sartorius LP220S, with a precision of 1 mg. For each TGA run, a platinum crucible filled with 2 grams of sample was heated with a constant heating rate of 25 °C per hour from 100 °C to the final chosen temperature (150 °C, 400 °C, 650 °C, 1000 °C, and 1300 °C), and held at this final temperature during one hour. At the end of TGA runs, samples were promptly removed from the furnace and stored in an oven to avoid any hydration from the ambient atmosphere. ICP-AES, ICP-MS and wet chemical methods were undertaken on these samples for bulk chemistry, while X-ray diffraction was used for mineralogical characterization.

For direct melting experiments, a platinum crucible was filled with 2 grams of sample, introduced into the center of the tube furnace, and directly heated from ambient (25 °C) to the dwell temperature (1400 °C), during 1 hour and 16 hours respectively. At the end of each experiment, the sample was drop-quenched in water, and analyzed in the same way as TGA samples.

2.4. Analytical methods

For the determination of melting temperature and crystallization sequence, polished thin sections of quenched samples were examined using a CAMECA SX-50 electron

microprobe equipped with 4 spectrometers and a wavelength-dispersive system (WDS), at the Université Henri Poincaré, Nancy 1. All WDS analyses were performed with a 15 kV accelerating voltage and 10.0 nA beam current. The following elements were analyzed: Na, Mg, Al, Si, P, S, Cl, K, Ca, Ti, Cr, Fe, Zn, and Pb. Electron microprobe standardization was conducted using polished geological standards prior to analyses. Incident-beam diameter was 10 μm on glass to minimize the volatilization of alkalis, whereas a focused beam was used on crystalline phases.

For bulk chemistry performed at the Service d'Analyse des Roches et des Minéraux (SARM, CRPG-CNRS), major elements (Si, Al, Fe, Mn, Mg, Ca, Na, K, Ti and P) were analyzed by inductively coupled plasma atomic emission spectroscopy (ICP-AES), chlorine by absorptiometry, fluorine by potentiometry, sulfur and carbon by impulsion coulometry. Concentrations of trace pollutant elements (As to Zn) were measured by inductively coupled plasma mass spectrometry (ICP-MS), except for mercury, analyzed by atomic absorption. Details of these chemical methods are given in a previous paper [5]. The relative uncertainties are 5 to 25 % for contents around 1 $\mu\text{g/g}$, 2 to 10 % for contents in the order of 10 $\mu\text{g/g}$, and 2 to 5 % above 100 $\mu\text{g/g}$.

For X-ray diffraction, a Jobin Yvon-Sigma 2080 diffractometer was used along with a copper X-ray source (38 kV, 20 mA, 800 W) on sample powder (< 50 μm). Scans were conducted from 2 to 32° at a rate of 0.5° of θ per minute. The diffractogram was evaluated for possible crystalline phases using the ASTM (American Society for Testing Materials) data base for pure species.

3. Results

3.1. Melting temperature and phase relations

The liquidus temperature of ESP ashes was determined either by the reading of appropriate phase diagram and by melting experiments performed in high temperature

furnace. Since ESP ashes are mainly constituted by SiO_2 , CaO , Al_2O_3 and Cl , with a total of around 75 wt.%, [3,5], and that chlorine is a highly volatile element, the melting products of fusion of ESP ashes can be properly represented in the ternary diagram $\text{CaO-SiO}_2\text{-Al}_2\text{O}_3$ [18]. All ESP ash compositions documented by Le Forestier and Libourel [5] were plotted in this diagram. These residues cluster in the same area, close to the gehlenite-anorthite cotectic curve, which confirms their homogeneous composition in term of major elements (Fig. 1). The direct reading of this phase diagram allows us to estimate the melting temperatures of ESP ashes in the range 1265 °C-1400 °C.

These ESP ashes were compared to another type of flue gas residues, a semi-dry scrubber residue (SDSR), obtained by semi-dry process, in which flue gas, after cooling, is cleaned by injection of a lime slurry into the scrubber. In the same diagram (Fig. 1), SDSR samples are scattered toward the CaO end-member, in response to lime injection in the scrubber to neutralize acid gases. Accordingly, their melting temperature varies between 1900 °C and 2300 °C, revealing the more refractory character of SDSR. Moreover, Fig. 1 shows that, despite the chemical and mineralogical discrepancies between SDSR and ESP ashes, their $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratio hardly varies outside 1.5 and 2.7. Assuming that these variations correspond to most of the flue gas residues, a temperature-composition section (T-X) can be drawn from this phase diagram to evaluate their liquidus temperature, simply as a function of their CaO content (Fig. 2).

In order to better constrain the melting temperatures of ESP ashes, a set of heating experiments was carried out on two different samples, for which experimental conditions are reported in Table 1. Experiments show that the liquidus temperature of ESP 261 and ESP 110 are in the range 1256-1272 °C and 1202-1256 °C, respectively.

In addition, these experiments allow to characterize the phase relationships below the liquidus temperature. For ESP 261, electron microprobe analyses reveal that the liquidus phase is a spinel, belonging to the solid solution between spinel *stricto sensu* and Zn-rich aluminous spinel related to franklinite, containing an average of 7.24 ± 0.39 wt.%

of Zn, 2.34 ± 0.29 wt.% of Fe, and 0.88 ± 0.47 wt.% of Cr. At 1225 °C, anorthite ($\text{CaAl}_2\text{Si}_2\text{O}_8$) joins spinel as a crystallizing phase, followed by melilite ($\text{Ca}_2\text{Mg}_{0.26}\text{Al}_{1.38}\text{Si}_{1.53}\text{O}_7$) at 1190 °C. Similar phase relationships were obtained for ESP 110.

3.2. Mass losses

Since solidification-stabilization processes may involve high temperature treatments, both chemical and mineralogical changes due to heating of ESP ash were investigated, using the coupling of thermogravimetric experiments, X-ray diffraction and chemical analyses.

Several thermogravimetric analyses (TGA) were performed on the representative ESP 261 sample between 100 °C and 1300 °C (Fig. 3), in order to characterize the associated mineralogical and chemical changes. The resulting thermogravimetric curves for final temperatures of 1300 °C, 1000 °C and 650 °C have the same shape, which confirms the reproductivity of mass loss, and indicate a total mass loss of around 18 wt.% at the final temperature of 1300 °C. In details, the TGA curves show an initial rapid decrease between 100 and 150 °C, followed by a less important mass loss in the range of 150 to 550 °C. After a step with no mass loss between 550 and 800 °C, we observe a significant decrease up to 1000 °C. Above this temperature, the mass loss remains weak up to the melting temperature, suggesting that around 90 % of the mass loss takes place before 1000 °C for this ESP ash.

X-ray diffractograms were carried out on the representative ESP 261 sample and on the by-products of each TGA experiments performed at 150 °C, 400 °C, 650 °C, 1000 °C, and 1300 °C, in order to relate these mass losses to mineralogical changes (Fig. 4). X-ray diffraction pattern reveals the occurrence of halite, sylvite, quartz, melilite, calcite, anhydrite, feldspar, and hematite in the selected ESP ash. However, our previous study devoted to the detailed characterization of MSW flue gas residues [5] has highlighted the

more complex mineralogy of ESP ashes with the occurrence of other silicates, carbonates, chlorides, sulphates, oxides, and also graphite, hydroxides (e.g. portlandite), phosphates, and metallic phases (e.g. Al, Zn). As shown by X-ray diffraction, TGA products obtained at 150 °C and 400 °C contain the same major phases as the initial ESP ash (Fig. 4). At 650 °C, corresponding to a relative mass loss of 11 wt.%, the mineralogy is clearly different, with the disappearance of chlorides (sylvite and halite) and calcite, and the crystallization of mayenite ($\text{Ca}_{12}\text{Al}_{14}\text{O}_{33}$). At 1000 °C, mayenite and anhydrite no longer exist, whereas the intensity of peaks for melilite and wollastonite (CaSiO_3) increases. Finally, all peaks of diffraction disappear in favour of amorphous bump at 1300 °C, which confirms the melting of ESP ashes in this temperature range (Fig. 1 and 2).

In addition, after TGA, all samples were analyzed by ICP-AES and ICP-MS, analytical results are reported in Table 2. By comparison with non-heated samples, these results reveal that, as expected, refractory elements concentrate in the most heated samples, while the reverse trend is observed for the volatile elements. For instance, Al, Ca and Ti contents increase with temperature, whereas Cl, S, Na, and K contents decline. Amongst the pollutant elements, Hg, Cd, Pb, and Cu are strongly depleted, whereas As, Co, Cr, Ni, Sb, Sn, and Zn remain in the residues.

Since the glass resulting from TGA experiment at 1300 °C was obtained after 48 hours of heating, additional melting experiments were performed on the same starting ESP 261 composition, in order to better simulate the vitrification occurring at an industrial scale. Experiments were carried out for 1 and 16 hours by direct melting of the sample at 1400 °C in air (Table 2). All experiments produced calcium-rich aluminosilicate glasses. Both calculated and measured mass losses are in good agreement, 19 wt.% for melting during TGA experiment at 1300 °C, and ~22 wt.% for direct melting at 1400 °C for 1 and 16 hours. These results show that, by comparison with the initial composition, the main changes of composition occur during the first hour, in accordance with the work of Jakob *et al.* [14] on similar flue gas residues.

4. Discussion

4.1. High temperature behavior of ESP ash

The relative amount of evaporation of elements can be calculated from the mass loss and the chemical composition, using the following expression:

$$E_{i,T} = 100 \cdot [1 - (m_T / m_0) \cdot (X_{i,T} / X_{i,0})]$$

where $E_{i,T}$ is the relative amount of evaporation of the element i at temperature T , m_T is the final mass measured at T , m_0 is the initial mass (2 grams), $X_{i,T}$ is the content of i in the product obtained after TGA up to T , and $X_{i,0}$ is the content of i in the initial ESP ash. Chemical analyses of the initial ESP ash and of each TGA product are given in Table 2, whereas relative amount of evaporation for major volatile elements as a function of temperature is represented in Fig. 5.

All together, these results allow to depict the high temperature behavior of these ESP ashes, in term of their mineralogy and chemistry. After the evaporation of 2.1 wt.% water before 150 °C, organic carbon has been oxidized to CO₂ and almost totally volatilized at 400 °C. The remaining carbon, given by difference between total carbon and organic carbon, is related to carbonates. According to Fig. 5a, this inorganic carbon is volatilized at 650 °C, due to the disappearance of calcite by decarbonation, as shown by X-ray diffractograms in Fig. 4. Similarly, the disappearance of chlorides (halite and sylvite) around 650 °C is supported by the similar behavior of alkali elements (Na and K) and chlorine, with a significant increase of their evaporation rate between 400 and 1000 °C. In the same temperature range, a calcium aluminate, i.e. mayenite (Ca₁₂Al₁₄O₃₃) formed (Fig. 4), very likely in response to the deshydration of portlandite or the decalcification of CaO-SiO₂-H₂O (CSH) phases and the oxidation of metallic aluminum. At 1000 °C, the mineralogy is dominated by melilite, quartz, feldspar and wollastonite. Raising the temperature up to 1000°C led to the development of wollastonite and melilite. This is in agreement with the

findings of Karoly *et al.* [19] who conducted heat treatment of MSW fly ashes at temperatures between 850 and 1050°C, however, using a previous melting at 1600°C followed by a cooling and annealing at 600°C. As shown in Fig. 5a, sulfur shows a contrasting behavior, by comparison with chlorine, and mainly vaporizes between 1000 and 1300 °C. After direct melting at 1190 °C of ESP ash, the main crystalline phases were identified as spinel, anorthite, and melilite. These parageneses, obtained at 1000 °C and 1190 °C, are in agreement with phase relationships at the eutectic point (1170 °C) in the ternary diagram CaO-SiO₂-Al₂O₃ (Fig. 1). Clozel and Legendre [20] have characterized the paragenesis of MSW flue gas residues heated at around 1200 °C. They have identified similar phases (spinel *stricto sensu*, melilite close to gehlenite, plagioclase), but also Ca rich-pyroxene and some minor phases such as apatite and perovskite. Moreover, our melting temperatures are in good agreement with Lin and Chang [17] for the melting of a cyclone ash (1250 °C), and a little above to those given by Jakob *et al.* [14] for MSWC fly ashes (1180 °C), because of higher amounts of refractory elements (Ca, Al, Mg) in our selected ESP ash.

The predicted liquidus temperatures, obtained by using the ternary diagram CaO-SiO₂-Al₂O₃, are in the same order of magnitude as the experimental ones, but a little higher. The small difference may be simply explained by the presence of minor elements which act as fluxes (e.g. Fe, Na, K, P). Therefore, predicted liquidus temperature based on the CaO-SiO₂-Al₂O₃ ternary diagram represents an upper limit for the melting of ESP ashes.

4.2. Specific behavior of pollutants

Concerning pollutant elements (Fig. 5b), all mercury has already volatilized at 400 °C. Metallic mercury Hg⁰ has very low boiling point, at 357 °C [21], and according to Galbreath and Zygarlicke [22], Hg⁰(g) is the thermodynamically stable form in the highest temperature regions of combustors. However, the high chlorine partial pressure prevailing during waste combustion may cause the oxidation of mercury, and chloride mercury

species may be the major form in the cooling process of flue gas, as shown by Ghorishi *et al.* [23], Chen *et al.* [24]. Lead, cadmium and copper show similar evaporation curves, with the principal volatilization between 650 and 1000 °C. For fine-grained fly ash, Jakob *et al.* [14] have found that more than 90 % of evaporation in air is obtained from 670 °C for Pb, 750 °C for Cd, and 850 °C for Cu. Considering the boiling points of Pb, Cd and Cu and their compounds (e.g. oxides, chlorides, sulphates) [21], we can deduce that (i) none of the oxides is volatile below 1000 °C, (ii) Pb and Cu metals are refractory, whereas Cd metal is volatile at 765 °C, (iii) sulphates of Cd and Pb are not volatile, and CuSO₄ is decomposed in CuO, (iv) chlorides of Pb, Cd and Cu are volatile below 1000 °C. As the high chlorine content in ESP ash will create an important partial pressure of chlorine during heating, chloride is the most probable form of evaporation for Pb, Cd and Cu. Fig. 5b shows a lesser evaporation for copper at high temperature, which can be explained by the occurrence of metallic alloys in addition with chloride copper.

For zinc, the relative amount of evaporation raises with increasing temperature from 0 % at 650 °C, 20 % at 1000 °C, and 1300 °C (Fig. 5b). The direct melting at 1400 °C during one hour reveals an evaporation of zinc at around 60 % (Table 2). Incomplete evaporation is found for zinc in air. That is in accordance with the crystallization of spinel, the stable phase at the liquidus, which contains more than 7 % of zinc. Jakob *et al.* [14] found also an increasing evaporation of zinc, up to 51 % at 1030 °C, but followed by a decrease to as low as 14 % at temperatures above the melting range of the filter ash. According to these authors, zinc exists in the form of oxide in the initial filter ash, and heating in air creates a competition between the formation of volatile zinc chloride and the formation of stable zinc silicate and zinc spinel. Struis *et al.* [25] have detailed the quantitative Zn speciation at different heat treatment stages, under Ar or Ar+O₂ carrier gas. Under O₂-enriched carrier gas, the Zn-bearing species of fly ash samples collected at different temperatures (400 °C, 765 °C and 910 °C) were identified as Zn₂SiO₄, ZnAl₂O₄, Zn₅(OH)₅(CO₃)₂, and ZnO. We suggest a complex crystal-chemistry of zinc in the initial

ESP ash, as shown by a previous study [5]: zinc was found as pure metallic particles, spinels, alloys, and Ca-bearing aluminosilicate glasses. It is noticeable that particles of zinc metal and alloys can have been partially oxidized during heating in air. So, the increase of evaporation of zinc is due to the different Zn-bearing species, which are very volatile (e.g. zinc metal) as well as refractory (e.g. spinel).

The other potentially toxic metals reveal a different behavior during heating, even if uncertainties of the calculated amounts of evaporation are higher due to the low contents of these metals in the fly ash residues. Chromium presents a negligible evaporation (Fig. 5b), and a similar trend was obtained for nickel, antimony and tin. No evidence was found concerning their main bearing phases, with the notable exception of Ni, for which spinel and metallic alloys were identified as potential Ni carrier.

5. Conclusions

The results presented in this study can be thus used as a guide for vitrification processes, especially for industrial furnace control. So, in industrial glassmaking furnaces using typically temperatures around 1400 °C, the direct vitrification of ESP ash is possible without any additives, because the silica content is enough to form a glass. On the contrary, semi-dry scrubber residues are more refractory with high amounts of calcium, and additives, such as Na_2CO_3 or SiO_2 , are necessary to melt these residues at lower temperatures than their melting one [26].

In addition to previous studies, our knowledge of polluting element behavior of MSW flue gas residues at high temperature has been significantly improved, leading to two different strategies for the management of MSW flue gas residues. In the first one, the objective is to promote the efficiency of the transfer of pollutant elements to the raw gas, in order to obtain vitrified products containing low amounts of toxic elements. In this case, these vitrified products, often called slags, may be used as secondary raw materials, such as

subbase in road construction or supplement for pavement. However and as shown in this paper, fumes obtained after vitrification concentrated the more toxic and volatile elements, which may create hazardous aerosols during condensation. In order to avoid such a transfer of pollution from the solid by-product of the incineration to the gas, fumes have therefore to be treated before their release in the atmosphere. In this alternative strategy, the challenge is to remove the soluble metals (e.g. Hg, Cd, Pb) from the MSW flue gas residues by an efficient leaching before vitrification, and to retain in an irreversible manner most of the remaining polluting elements in the vitrified products, either in the glassy matrix or better in stable crystalline phases, like spinels for Cr, Ni, Zn. Since during storage or reuse of these vitrified products the risk of release of toxic metals in the environment remains a threat, it is clear that their long-term durability has to be investigated, as well.

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References

- [1] R.R. Greenberg, W.H. Zoller, G.E. Gordon, Composition and size distributions of particles released in refuse incineration, *Environ. Sci. Technol.* 12 (1978) 566-573.
- [2] J.L. Ontiveros, T.L. Clapp, D.S. Kosson, Physical properties and chemical species distributions within municipal waste combustor ashes, *Environ. Prog.* 8 (1989) 200-206.

- [3] A. Plüss, R.E. Ferrell, Characterization of lead and other heavy metals in fly ash from municipal waste incinerators, *Hazard. Waste Hazard. Mater.* 8 (1991) 275-292.
- [4] A. Goldin, C. Bigelow, P.L.M. Veneman, Concentrations of metals in ash from municipal solid waste combustors, *Chemosphere* 24 (1992) 271-280.
- [5] L. Le Forestier, G. Libourel, Characterization of flue gas residues from municipal solid waste combustors, *Environ. Sci. Technol.* 32 (1998) 2250-2256.
- [6] J. Carignan, G. Libourel, C. Cloquet, L. Le Forestier, Lead isotopic composition of fly ash and flue gas residues from municipal solid waste combustors in France: implications for atmospheric lead source tracing, *Environ. Sci. Technol.* 39 (2005) 2018-2024.
- [7] C.A. Cahill, L.W. Newland, Comparative efficiencies of trace metal extraction from municipal incinerator ashes, *Intern. J. Environ. Anal. Chem.* 11 (1982) 227-239.
- [8] I.A. Legiec, C.A. Hayes, D.S. Kosson, Continuous recovery of heavy metals from MSW incinerator ashes, *Environ. Prog.* 8 (1989) 212-217.
- [9] S. Cernushi, M. Giugliano, I. de Paoli, Leaching of residues from MSW incineration, *Waste Management & Research* 8 (1990) 419-427.
- [10] S.S. Krishnan, R.E. Jervis, L.D. Vela, Leachability of toxic elements from solid wastes, *Journal of Radioanalytical and Nuclear Chemistry* 161 (1992) 181-187.
- [11] C.S. Kirby, J.D. Rimstidt, Interaction of municipal solid waste ash with water, *Environ. Sci. Technol.* 28 (1994) 443-451.
- [12] T.T. Eighmy, J.D. Eusden, J.E. Krzanowski, D.S. Domingo, D. Stämpfli, J.R. Martin, P.M. Erickson, Comprehensive approach toward understanding element speciation and leaching behavior in municipal solid waste incineration electrostatic precipitator ash, *Environ. Sci. Technol.* 29 (1995) 629-646.
- [13] P.P. Bosshard, R. Bachofen, H. Brandl, Metal leaching of fly ash from municipal waste incineration by *Aspergillus niger*, *Environ. Sci. Technol.* 30 (1996) 3066-3070.

- [14] A. Jakob, S. Stucki, P. Kuhn, Evaporation of heavy metals during the heat treatment of municipal solid waste incinerator fly ash, *Environ. Sci. Technol.* 29 (1995) 2429-2436.
- [15] A. Jakob, S. Stucki, R.P.W.J. Struis, Complete heavy metal removal from fly ash by heat treatment: influence of chlorides on evaporation rates, *Environ. Sci. Technol.* 30 (1996) 3275-3283.
- [16] S.I. Sakai, M. Hiraoka, Municipal solid waste incinerator residue recycling by thermal processes, *Waste Manage.* 20 (2000) 249-258.
- [17] K.L. Lin, C.T. Chang, Leaching characteristics of slag from the melting treatment of municipal solid waste incinerator ash, *J. Hazard. Mater. B135* (2006) 296-302.
- [18] E.M. Levin, C.R. Robbins, H.F. Mc Murdie, *Phase Diagrams for Ceramists*, third ed., American Ceramics Society, Columbus, Ohio, 1964.
- [19] Z. Karoly, I. Mohai, M. Toth, F. Weber, J. Szepvölgyi, Production of glass-ceramics from fly ash using arc plasma, *J. Eur. Ceram. Soc.* 27 (2007) 1721-1725.
- [20] B. Clozel, O. Legendre, Caractérisation minéralogique et cristalochimique de vitrifiats, *Proceedings of the International Congress on Waste Solidification-Stabilisation Processes*, 28 november-1st december 1995, Nancy, France, 1997, pp. 53-57.
- [21] R.C. Weast, M.J. Astle, W.H. Beyer, *Handbook of Chemistry and Physics*, 69th ed., CRC Press, Boca Raton, Florida, 1988-1989.
- [22] K.C. Galbreath, C.J. Zygarlicke, Mercury speciation in coal combustion and gasification flue gases, *Environ. Sci. Technol.* 30 (1996) 2421-2426.
- [23] S.B. Ghorishi, C.W. Lee, W.S. Jozewicz, J.D. Kilgroe, Effects of fly ash transition metal content and flue gas HCl/SO₂ ratio on mercury speciation in waste combustion, *Environ. Eng. Sci.* 22 (2005) 221-231.

- [24] L. Chen, Y. Zhuo, X. Zhao, Q. Yao, L. Zhang, Thermodynamic comprehension of the effect of basic ash compositions on gaseous mercury transformation, *Energ. Fuel* 21 (2007) 501-505.
- [25] R.P.W.J. Struis, C. Ludwig, H. Lutz, A.M. Scheidegger, Speciation of zinc in municipal solid waste incineration fly ash after heat treatment: an X-ray absorption spectroscopy study, *Environ. Sci. Technol.* 38 (2004) 3760-3767.
- [26] Y.J. Park, J. Heo, Vitrification of fly ash from municipal solid waste incinerator, *J. Hazard. Mater.* B91 (2002) 83-93.
- [27] R. Kretz, Symbols for rock-forming minerals, *Am. Mineral.* 68 (1983) 277-279.

Fig. 1. Liquidus surface, sub-solidus equilibria, and location of the electrostatic precipitator (ESP) ash and semi-wet scrubber residues (SDSR) samples in the $\text{CaO-SiO}_2\text{-Al}_2\text{O}_3$ system [18].

Fig. 2. Diagram showing the theoretical and experimental liquidus temperature of flue gas residues as a function of their CaO content, for two $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratios, 1.5 and 2.7 respectively. This diagram corresponds to sections through the phase diagram in the $\text{CaO-SiO}_2\text{-Al}_2\text{O}_3$ system.

Fig. 3. Weight loss curves obtained by thermogravimetric analysis (TGA) of the selected electrostatic precipitator ash ESP 261. TGA 1300, TGA 1000 and TGA 650 correspond to thermogravimetric curves for final temperatures of 1300, 1000, and 650 °C, respectively. TGA, thermogravimetric analysis.

Fig. 4. X-ray diffraction patterns of the selected electrostatic precipitator ash ESP 261, and of run products obtained after thermogravimetric analysis (TGA) measurements. TGA 150, TGA 400, TGA 650, and TGA 1000 correspond to run products obtained after TGA for final temperatures of 150, 400, and 1000 °C, respectively. TGA, thermogravimetric analysis; Hl = halite; Syl = sylvite; Qtz = quartz; Cal = calcite; Anh = anhydrite; Mel = melilite; Fs = feldspar; Hem = hematite; May = mayenite; Wo = wollastonite. Symbols used for synthetic solid phases related to minerals are those of Kretz [27].

Fig. 5. Relative amount of evaporation as a function of temperature, (a) of the volatile elements Na, K, Rb, Cs, Cl, S, C, TOC (total organic carbon), and (b) of the pollutant elements Hg, Cd, Pb, Cu, Zn, Cr, for the selected electrostatic precipitator ash ESP 261. The heat treatment of this ESP ash, performed in air, consists of thermogravimetric

measurements for 150, 400, 650, 1000, and 1300 °C, and direct melting for 1350, 1400, and 1500 °C.

Table 1. Phases relationship experimental conditions for two representative fly ashes

Run	Raw material	Duration (hours)	Temperature (°C)	Phases present in the sample
CEL2	ESP 261	4	1350	Glass
CEL1	ESP 261	1	1290	Glass
CEL8	ESP 261	1	1272	Glass
CEL9	ESP 261	1	1256	Glass + Spl ^a
CEL5	ESP 261	24	1240	Glass + Spl
CEL10	ESP 261	1	1225	Glass + Spl + An ^b
CEL7	ESP 261	24	1190	Glass + Spl + An + Mel ^c
CEL8	ESP 110	1	1272	Glass
CEL9	ESP 110	1	1256	Glass
CEL11	ESP 110	1	1202	Glass + Spl + An + Mel

^aSpl = spinel $(\text{Mg}_{0.82}\text{Zn}_{0.18})(\text{Al}_{1.91}\text{Fe}_{0.06}\text{Cr}_{0.03})\text{O}_4$. ^bAn = anorthite $\text{CaAl}_2\text{Si}_2\text{O}_8$. ^cMel = melilite $\text{Ca}_2\text{Mg}_{0.26}\text{Al}_{1.38}\text{Si}_{1.53}\text{O}_7$.

Table 2. Chemical composition of the selected electrostatic precipitator ash, ESP 261, of the products TGA i obtained by heating ESP 261 up to i °C, and of the glasses, DM 1h 1400 and DM 16h 1400, obtained after direct melting of ESP 261 at 1400 °C during 1 and 16 hours, respectively.

	ESP 261	TGA ^a 150	TGA 400	TGA 650	TGA 1000	TGA 1300	DM 1h 1400	DM 16h 1400
Mass ^b (mg)	2000	1958	1915	1830	1690	1643		
Mass loss ^c (%)		2.10	4.25	8.50	15.50	17.85 19 ^d	22	22
Si (wt.%)	13.57	13.75	14.34	15.77	16.78	16.78	17.36	17.14
Al (wt.%)	8.85	8.98	9.40	10.47	11.20	11.32	12.22	12.27
Fe (wt.%)	1.20	1.22	1.38	1.21	1.31	1.33	0.67	0.91
Mn (wt.%)	0.08	0.09	0.09	0.09	0.10	0.11	0.08	0.08
Mg (wt.%)	1.78	1.83	1.89	2.18	2.22	2.22	2.30	2.22
Ca (wt.%)	15.94	16.14	16.52	18.07	18.88	19.95	20.48	20.31
Na (wt.%)	2.40	2.46	2.18	1.73	1.70	1.09	1.26	1.05
K (wt.%)	3.35	3.35	3.01	2.20	1.15	0.58	0.37	0.29
Ti (wt.%)	1.00	1.02	1.06	1.14	1.25	1.24	1.22	1.22
P (wt.%)	0.55	0.50	0.59	0.61	0.68	0.66	0.61	0.63
LOI ^e (wt.%)	16.93	15.85	13.51	7.38	2.38	0.15	n.d.	n.d.
Cl (wt.%)	6.58	6.50	5.37	3.81	0.70	0.01	0	0
S (wt.%)	0.90	0.85	0.97	0.94	0.75	0.02	0	0
total C (wt.%)	3.08	3.28	1.04	0.15	0.04	n.d.	n.d.	n.d.
TOC ^f (wt.%)	2.63	2.73	0.25	n.d. ^g	n.d.	n.d.	n.d.	n.d.
As (ppm)	18	19	19	21	22	22	14	6
Cd (ppm)	115	117	118	116	11	6	7	3
Co (ppm)	16	18	18	19	21	21	14	15
Cr (ppm)	371	373	397	364	448	425	304	148
Cu (ppm)	792	790	800	854	265	84	97	71
Hg (ppm)	14	14.4	0.6	n.d.	n.d.	n.d.	n.d.	n.d.
Ni (ppm)	67	68	71	62	74	74	30	28
Pb (ppm)	1914	2246	2286	1503	225	128	645	240
Sb (ppm)	284	302	302	317	317	333	240	211
Sn (ppm)	787	802	805	835	830	889	708	915

Zn (ppm)	5044	5101	5153	5620	4748	5224	1831	2483
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^aTGA, thermogravimetric analysis. ^bThis mass corresponds to the initial mass for ESP and to the final mass obtained after each TGA. ^cMass loss = 100.(initial mass - final mass) / initial mass. ^dIn *italic*, the calculated mass loss (%) = 100 . [1 – (X_{Si,ESP ash} / X_{Si,Glass})].

^eLOI = loss on ignition at 980 °C. ^fTOC = total organic carbon. ^g n.d. = not determined.

Fig. 1

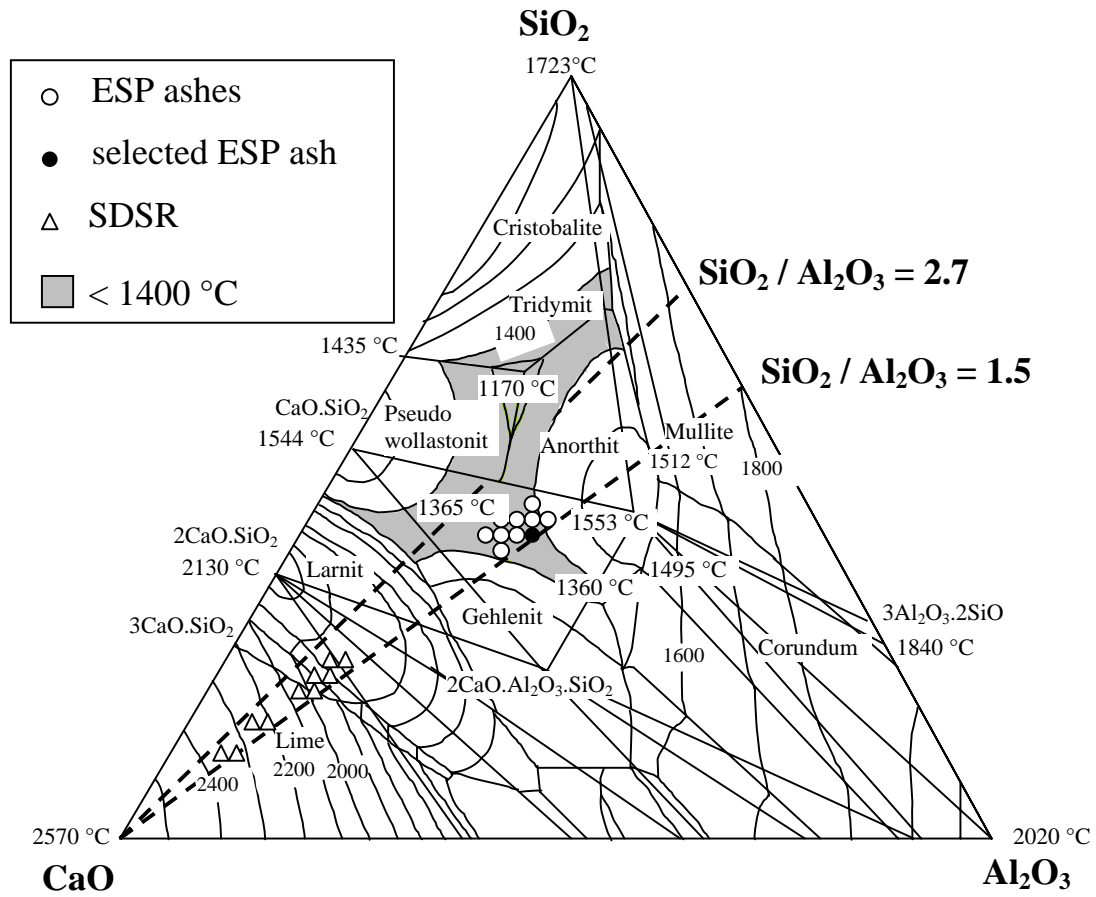


Fig. 2

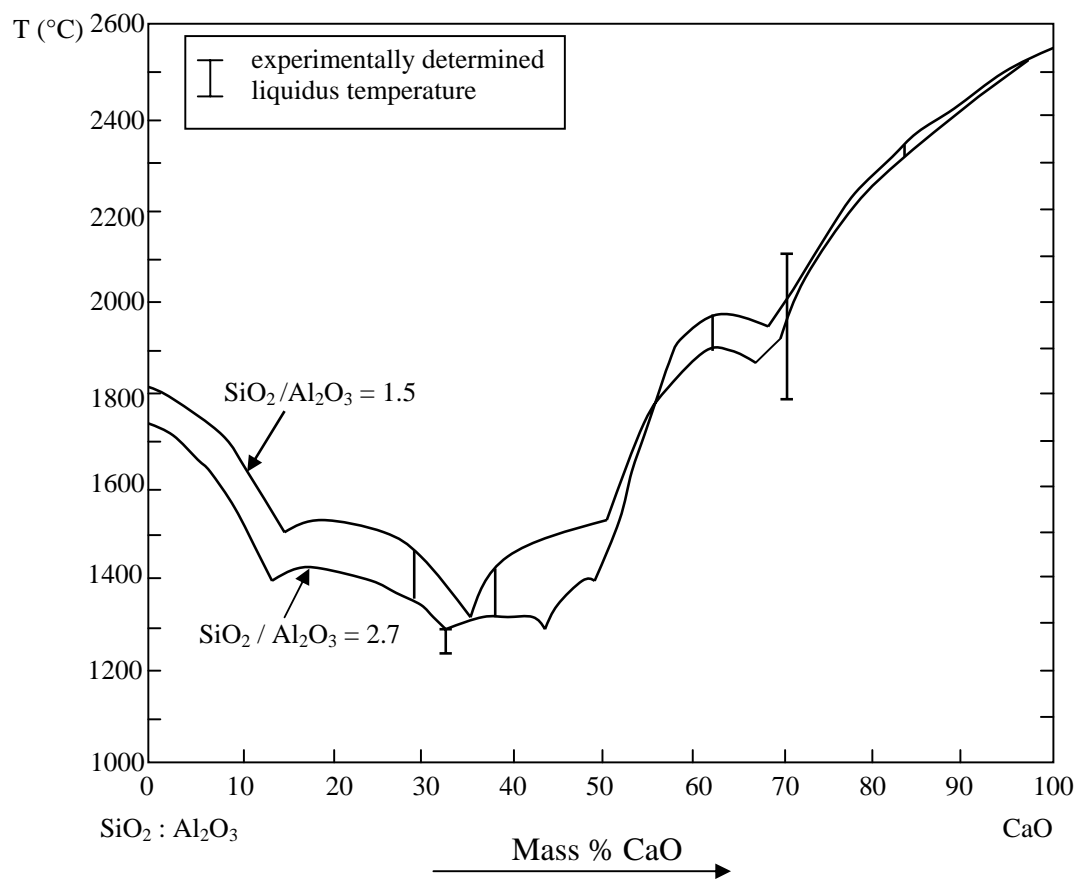


Fig. 3

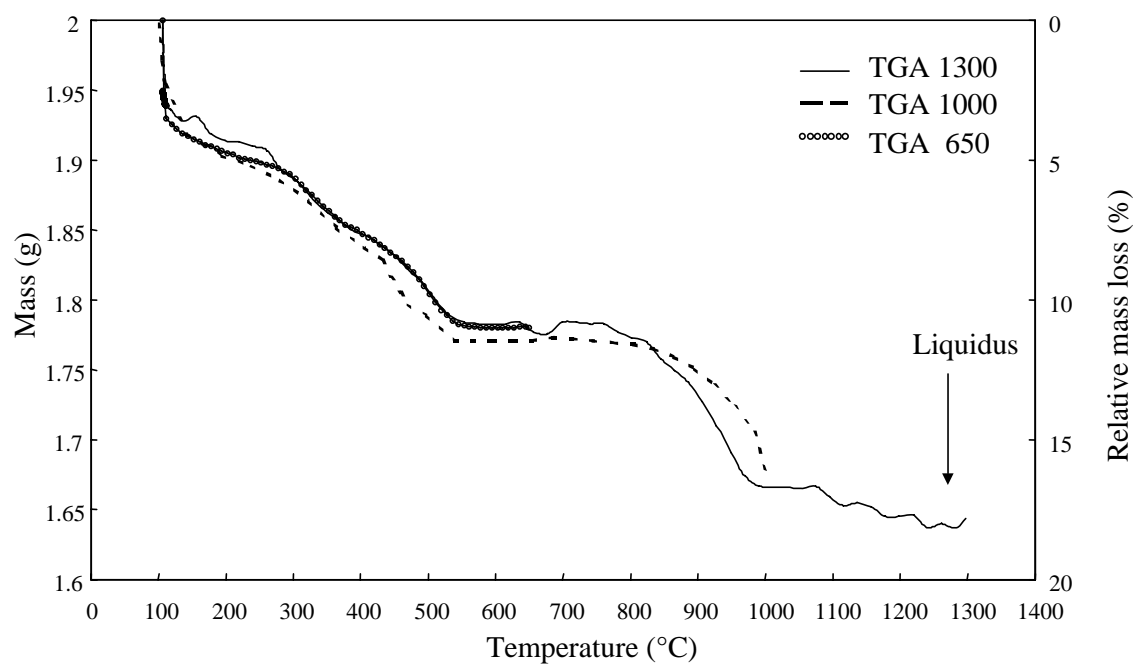


Fig. 4

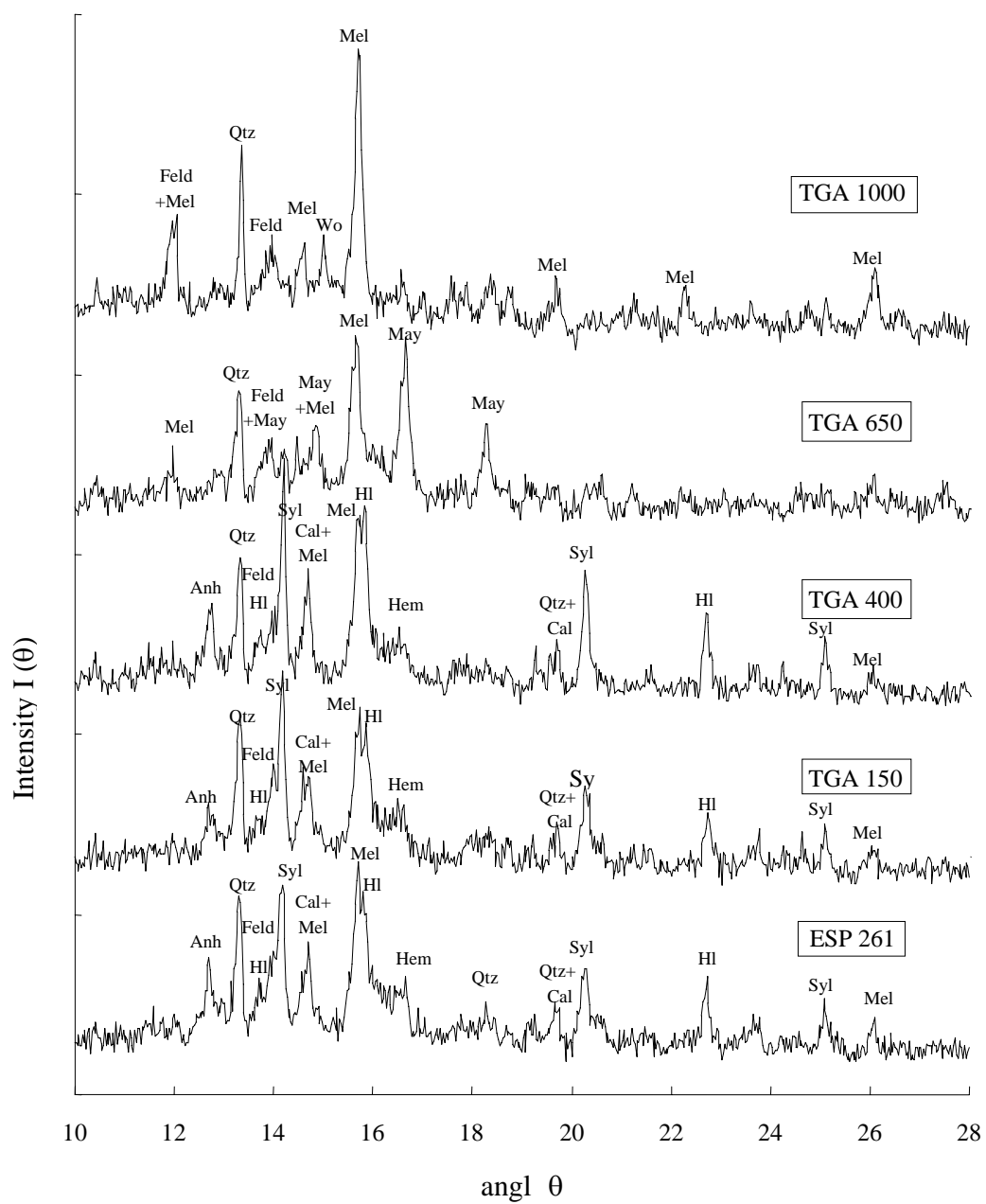


Fig. 5a

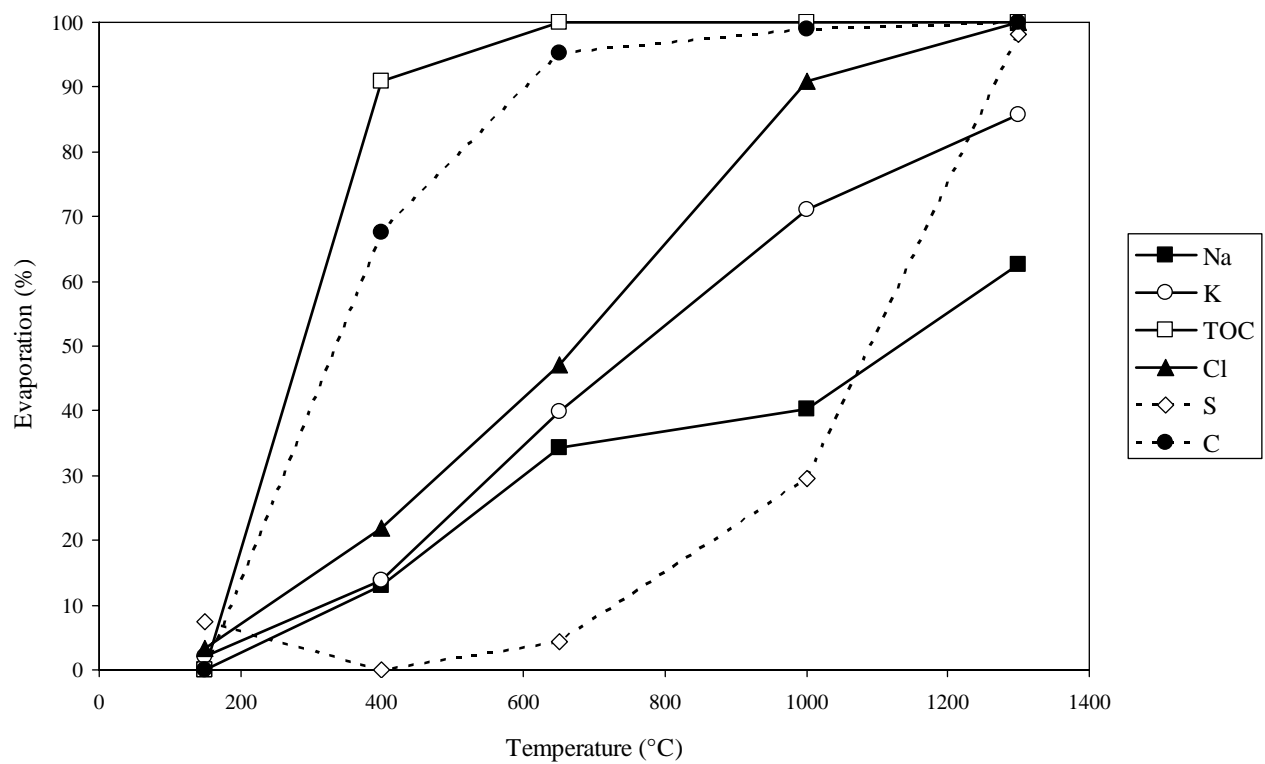


Fig. 5b

